

Production of Electricity and/or Fuels from Biomass by Thermochemical Conversion

Eric D. Larson*
Haiming Jin**
Fuat Celik*

RBAEF Meeting
Washington, DC
23 February 2004

* Princeton Environmental Institute
Princeton University
Princeton, NJ

** Thayer School of Engineering
Dartmouth College
Hanover, NH

Tasks 2 & 3: Conversion Technology

- a. Power generation
 - b. Thermochemical fuels (TCFs)
 - c. Ethanol
 - d. Mobility chain analysis
 - e. Environment analysis
- Dartmouth: Lee Lynd, Mark Laser, Haiming Jin, Kemantha Jayawardhana, Charles Wyman
 - Princeton: Eric Larson, Fuat Celik
 - NREL: John Sheehan
 - Argonne Lab: Michael Wang
 - NRDC: Nathanael Greene, Dan Saccardi
-
- ```
graph LR; subgraph Group1; A[a. Power generation]; B[b. Thermochemical fuels (TCFs)]; C[c. Ethanol]; end; D[d. Mobility chain analysis]; E[e. Environment analysis]; Dartmouth[Dartmouth: Lee Lynd, Mark Laser, Haiming Jin, Kemantha Jayawardhana, Charles Wyman]; Princeton[Princeton: Eric Larson, Fuat Celik]; NREL[NREL: John Sheehan]; Argonne[Argonne Lab: Michael Wang]; NRDC[NRDC: Nathanael Greene, Dan Saccardi]; Group1 --- Dartmouth; Group1 --- Princeton; NREL --> D; NRDC --> E;
```

# Power, TCFs, and Ethanol: Overview

## Objectives

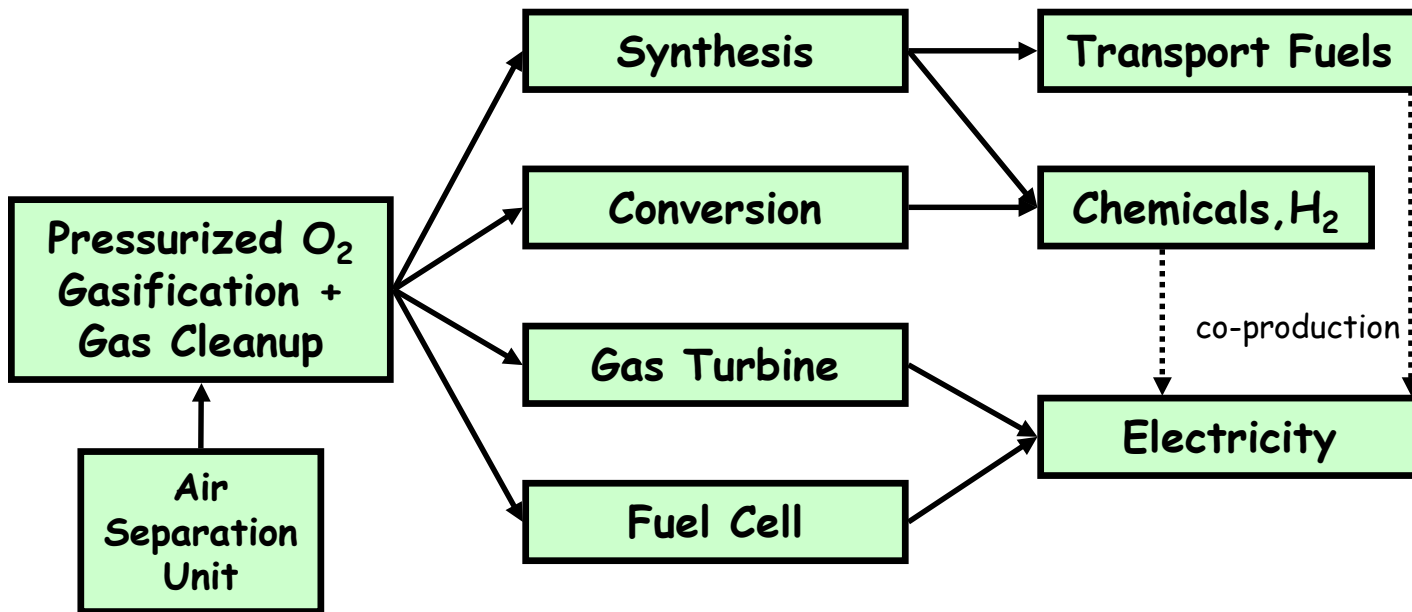
- Design self-consistent set of future, mature-technology processes for producing electricity and/or fuels (and chemicals, animal feed).
- Estimate performance and capital and operating costs.

## Approach

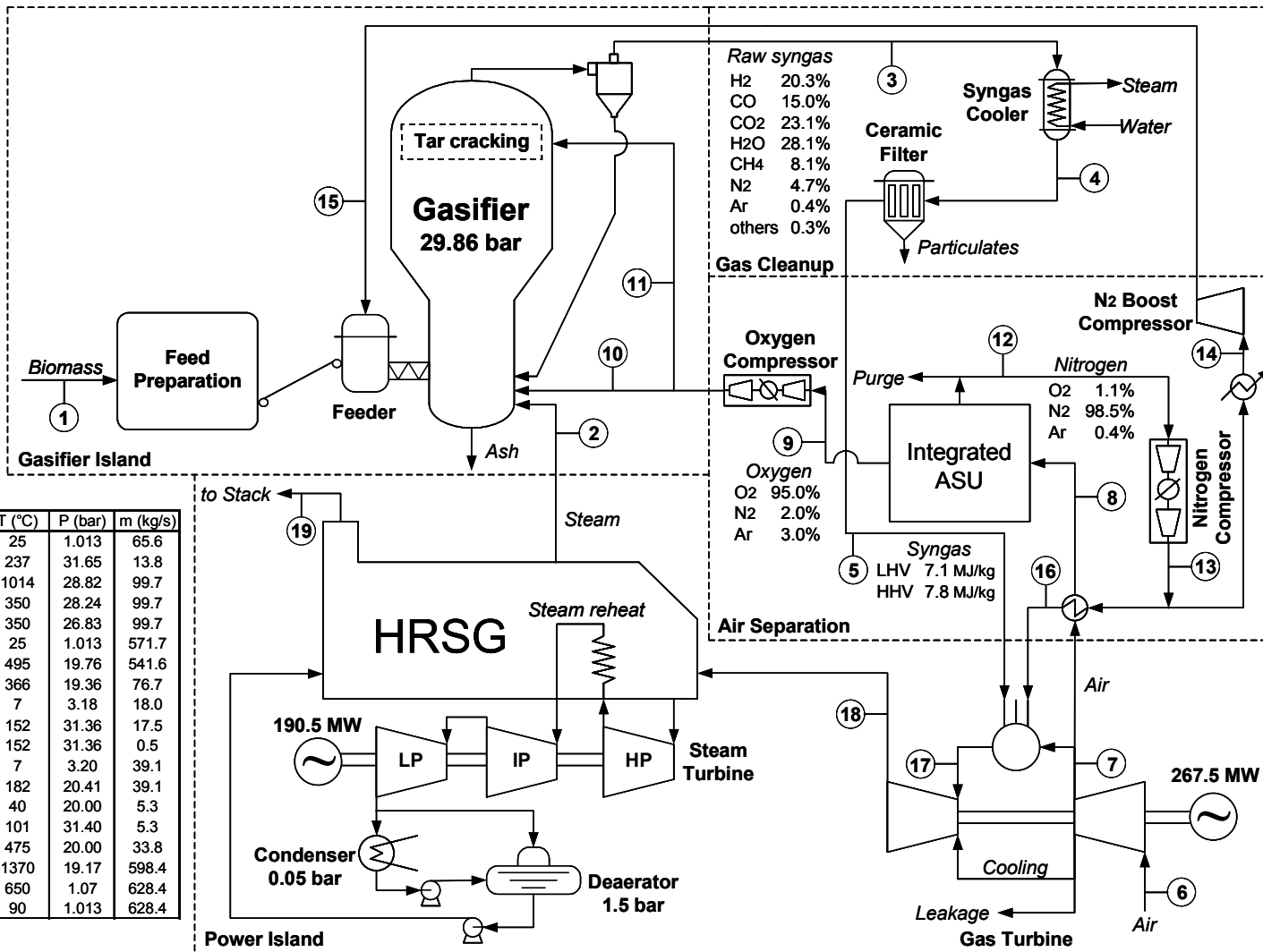
- Integrated effort between Dartmouth (biological) and Princeton (thermochemical)
- Design/simulation of heat and mass balances using Aspen<sup>+</sup>, with design parameter values from literature and experts.
  - RBAEF hypothesis: future mature biomass facilities will be relatively large (~5000 dry tons per day feed, or ~1000 MW<sub>th</sub>)
- Capital and operating cost estimates based on careful review of literature, own prior work, extensive discussion with industry experts, NREL cost database.
- Consistent financial parameters and accounting framework for economic analysis.
- Substantial effort: 20-25 Aspen<sup>+</sup> simulations in all !

# Thermochemical Conversion

High temperature (900-1000°C) gasification of biomass to make "synthesis gas" that subsequently is converted into electricity and/or fuels, chemicals, heat.



# Pressurized-Gasifier Combined Cycle



**Raw syngas**

|        |       |
|--------|-------|
| H2     | 20.3% |
| CO     | 15.0% |
| CO2    | 23.1% |
| H2O    | 28.1% |
| CH4    | 8.1%  |
| N2     | 4.7%  |
| Ar     | 0.4%  |
| others | 0.3%  |

**Oxygen**

|    |       |
|----|-------|
| O2 | 95.0% |
| N2 | 2.0%  |
| Ar | 3.0%  |

**Nitrogen**

|    |       |
|----|-------|
| O2 | 1.1%  |
| N2 | 98.5% |
| Ar | 0.4%  |

|    | T (°C) | P (bar) | m (kg/s) |
|----|--------|---------|----------|
| 1  | 25     | 1.013   | 65.6     |
| 2  | 237    | 31.65   | 13.8     |
| 3  | 1014   | 28.82   | 99.7     |
| 4  | 350    | 28.24   | 99.7     |
| 5  | 350    | 26.83   | 99.7     |
| 6  | 25     | 1.013   | 571.7    |
| 7  | 495    | 19.76   | 541.6    |
| 8  | 366    | 19.36   | 76.7     |
| 9  | 7      | 3.18    | 18.0     |
| 10 | 152    | 31.36   | 17.5     |
| 11 | 152    | 31.36   | 0.5      |
| 12 | 7      | 3.20    | 39.1     |
| 13 | 182    | 20.41   | 39.1     |
| 14 | 40     | 20.00   | 5.3      |
| 15 | 101    | 31.40   | 5.3      |
| 16 | 475    | 20.00   | 33.8     |
| 17 | 1370   | 19.17   | 598.4    |
| 18 | 650    | 1.07    | 628.4    |
| 19 | 90     | 1.013   | 628.4    |

Switchgrass input = 983 MW<sub>hhv</sub>

Net electric output = 443 MW<sub>e</sub>

Efficiency (HHV) = 45.1%

|                                      |                            |       |
|--------------------------------------|----------------------------|-------|
| Switchgrass input, MW <sub>hhv</sub> | Higher heating value (HHV) | 983.2 |
|                                      | Lower heating value (LHV)  | 886.8 |
| Internal power use, MW <sub>e</sub>  | ASU power <sup>a</sup>     | -6.4  |
|                                      | O2 compressor power        | 5.3   |
|                                      | N2 compressor power        | 10.8  |
|                                      | N2 boost compressor power  | 0.33  |
|                                      | Steam cycle pumps, total   | 3.5   |
|                                      | Fuel handling              | 0.66  |
|                                      | Lock hopper/Feeder         | 0.52  |
|                                      | Total on-site use          | 14.8  |
| Gross power output, MW <sub>e</sub>  | Gas turbine output         | 267.5 |
|                                      | Steam turbine gross output | 190.3 |
|                                      | Total gross output         | 457.8 |
| Net Power, MW <sub>e</sub>           |                            | 443.0 |
| Electricity efficiency, %            | Higher heating value (HHV) | 45.1% |
|                                      | Lower heating value (LHV)  | 50.0% |

# Key Technical Features Assumed for Mature Electricity Plants

- Reliable biomass feeding to pressurized gasifier.
- High reliability commercial gasifier operation.
- Acceptable extent of tar cracking.
- Warm-gas cleanup of particulates, alkali, trace contaminants and (for solid-oxide fuel cell) sulfur.
- Commercially reliable air separation unit integrated with gas turbine.
- Targeted solid-oxide fuel cell performance.

# Thermochemical Fuels (TCF)

## Fischer-Tropsch Liquids

(straight-chain  $C_nH_{2n}$ ,  $C_nH_{2n+2}$ )

- F-T fuels are commercially made from natural gas and (in S. Africa) from coal.
- F-T process dates to 1930s, but technology has improved significantly.
- Commercial fuel interest today is primarily in the middle distillate fraction, a high-cetane, no-sulfur diesel fuel substitute.
- The process also gives a naphtha fraction (chemical feedstock) and heavy waxes (high-value, small market).

## Dimethyl Ether

( $CH_3OCH_3$ )

- Ozone-safe aerosol propellant, chemical feedstock.
- Current global production < 150,000 tons/year by drying methanol ( $CH_3OH$ ).
- Similar to LPG – mild pressurization needed to keep as liquid.
- Good diesel-engine fuel: high cetane #, no sulfur, lower  $NO_x$ , no C-C bonds → no soot.
- Growing interest (especially in Japan, China, Sweden) for using DME

## Hydrogen

( $H_2$ )

- Intense  $H_2$  interest today.
- Preferred fuel for a fuel cell vehicle.
- Low or no tailpipe emissions of criteria pollutants or  $CO_2$ .
- Low volumetric energy density presents challenge for on-board storage.

## Methanol

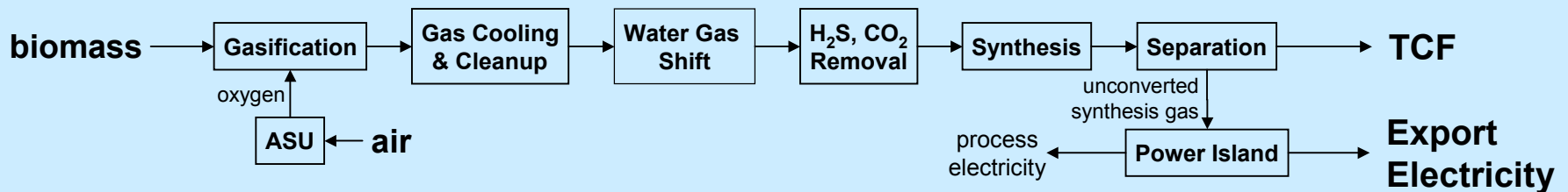
( $CH_3OH$ )

- Fuel cell vehicle fuel via onboard reforming.
- Health concerns as fuel.
- Chemical feedstock.

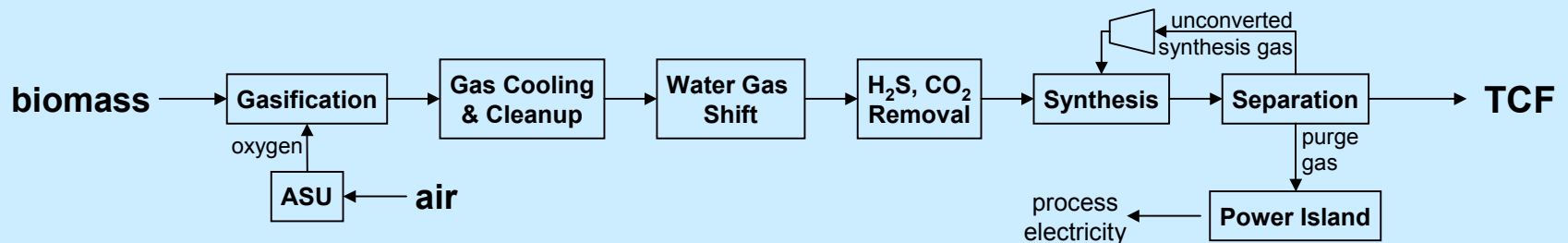
# Biomass Thermochemical Fuels (TCF)

- No commercial TCF production from biomass conversion today, but components are commercial or near commercially-ready.

## Design with “Once-Through” Synthesis



## Design with “Recycle” Synthesis



# Status of Process Simulations

| GASIFIER DESIGN →                        | Indirect, Atm-Pressure (BCL) | Pressurized Oxygen (GTI) |
|------------------------------------------|------------------------------|--------------------------|
| Gas turbine/steam turbine combined cycle | ●                            | ●                        |
| Solid-oxide fuel cell/gas turbine hybrid | ×                            | ●                        |
| Fischer-Tropsch Fuels                    | ×                            | ○                        |
| Fischer-Tropsch Fuels / Electricity      | ×                            | ○                        |
| Dimethyl Ether *                         | ×                            | ◐                        |
| Dimethyl ether / Electricity *           | ×                            | ◐                        |
| Hydrogen *                               | ×                            | ○                        |
| Hydrogen / Electricity *                 | ×                            | ○                        |
| Methanol                                 | ×                            | ◐                        |
| Methanol / Electricity                   | ×                            | ◐                        |
| Reference Rankine cycle                  | ●                            |                          |

\* Relatively pure stream of CO<sub>2</sub> is available as a byproduct in these cases, but the possibility of capture/storage of CO<sub>2</sub> as GHG emissions reduction option is not being considered in this project.

# Status of Cost Estimates

| GASIFIER DESIGN →                        | Indirect, Atm-Pressure (BCL) | Pressurized Oxygen (GTI) |
|------------------------------------------|------------------------------|--------------------------|
| Gas turbine/steam turbine combined cycle | ●                            | ●                        |
| Solid-oxide fuel cell/gas turbine hybrid | ×                            | ?                        |
| Fischer-Tropsch Fuels                    | ×                            | ○                        |
| Fischer-Tropsch Fuels / Electricity      | ×                            | ○                        |
| Dimethyl Ether *                         | ×                            | ◐                        |
| Dimethyl ether / Electricity *           | ×                            | ◐                        |
| Hydrogen *                               | ×                            | ○                        |
| Hydrogen / Electricity *                 | ×                            | ○                        |
| Methanol                                 | ×                            | ◐                        |
| Methanol / Electricity                   | ×                            | ◐                        |
| Reference Rankine cycle                  | ●                            |                          |

\* Relatively pure stream of CO<sub>2</sub> is available as a byproduct in these cases, but the possibility of capture/storage of CO<sub>2</sub> as GHG emissions reduction option is not being considered in this project.